1 Numerical simulation on Heat Extraction Performance of

2 Enhanced Geothermal System under the Different Well layout

10Abstract

11 China has hundreds of thousands of oil and water wells, about 30 percent of which have been 12abandoned currently. If we can convert abandoned wells into geothermal wells, it will save lots of 13money and reduce drilling and completion time greatly. In this paper, six enhanced geothermal 14system (EGS) well layout schemes are proposed based on the utilization of abandoned oil-water 15wells and common oilfield well pattern. Six common injection-production well pattern in oilfield 16 are combined to hot dry rock (HDR) production and the heat extraction performance is simulated. 17The results show that the injection well number and the location of injection wells have critical 18 influence on the heat extraction performance. Under the same total injection mass flow rate, the 19injection well number is the key factor and the fracture area is the secondary factor on heat 20 extraction when the HDR energy is enough. For electricity generation, the life span is 20.2, 19.2, 2119.0, 19.2, 18.2 and 13.9 years, the heat extraction ratio is 65.83, 57.35, 65.96, 62.79, 59.30 and 2243.09 % from case 1 to case 6, respectively. For heating demand, the life span is 30.0, 30.0, 29.9, 2330.0, 29.8, and 27.7 years, the heat extraction ratio is 78.91, 69.63, 77.02, 75.92, 72.27 and 58.94 24% from case 1 to case 6, respectively. The total injection mass flow rate and injection temperature 25also have the negative effect on the heat extraction performance. Case 1 (row parallel well layout), 26Case 3 (four-spot well layout) and Case 4 (five-spot well layout) is the good choice both for 27 electricity generation and heating demand. This study provides good guidance for the selection 28and optimization of different EGS well layout.

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32Keywords

33Hot Dry Rock, Enhanced Geothermal System, Well layout, Abandoned oil-water wells, Thermal-34Hydraulic model

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38Introduction

In recent years, with the increase of energy consumption and the intensification of greenhouse 2effect, clean energy plays an increasingly important role in the energy field (Ahmadi et al., 2018; 3Ramezanizadeh et al. 2019). Hot Dry Rock is a kind of deep geothermal resource which is clean 4renewable and widely distributed (Lu, 2018; Li et al., 2019; Wang et al., 2019). Compared with 5solar, wind and tidal power, the exploitation of HDR is less affected by the environmental factors 6(Li et al., 2015; Zhang et al., 2019). EGS extracts heat from HDR reservoir through fluid injection 7and it is considered to be an important way to exploit HDR (Moya et al., 2018). Considering the 8environmental impacts and economic benefits, EGS is considered to be the best way for electricity 9generation (Xu et al., 2018). However, the establishment of EGS is a costly and complicated 10system engineering, reducing the cost and difficulty is an important way to accelerate the HDR 11development (Pan et al., 2018).

12 China has hundreds of thousands of oil and water wells, about 30 percent of which have been 13abandoned currently (Bu et al., 2012). If we can convert abandoned wells into geothermal wells, it 14will save lots of money and reduce drilling and completion time greatly (Caulk et al., 2017; Cheng 15et al., 2014; Davis et al., 2009). At the same time, the extracted heat can be used for oil 16exploitation and transportation and power supply for nearby oilfield (Kharseh et al., 2019). 17Moreover, there is a strong correlation between geothermal and oil-gas production. The data 18information of oil and gas exploration, drilling, completion and exploitation can be used for 19geothermal development and utilization (Nian et al., 2018; Yang et al., 2017). In this paper, six 20EGS well layout schemes are proposed based on the utilization of abandoned oil-water wells and 21common oilfield well pattern. Six common injection-production well pattern in oilfield are 22combined to HDR production and the heat extraction performance is simulated.

23 A proper selection of well layout may reduce the development cost and increase the heat 24 extraction ratio (Ding et al., 2018; Li et al., 2018). The heat extraction performance of many kinds 25of well layout has been investigated currently. Yang et al. (2019) modeled the heat energy 26extraction performance in a triplet well layout and demonstrated that the well spacing, well radius, 27 reservoir thickness and injection mass flow rate affect the heat extraction ratio significantly. Chen 28et al. (2017) simulated the heat extraction performance of doublet, triplet, quintuplet well layout 29and found that simply increasing the production well number is not necessary to improve the heat 30extraction performance of EGS, triplet well layout can perform better than quintuplet well layout 31or worse than an EGS with the standard doublet well layout. Xia et al. (2017) simulated horizontal 32doublet well layout which parallel injection and production wells connected by a set of single 33large wing fractures and proposed that 40 equidistant fractures along 1.2 km long parallel well 34section with well distance of 500 m would meet the industrial production-level system. There are 35many single-well geothermal systems, such as heat pipe single well (Huang et al., 2018), 36multilateral-well (Shi et al., 2019), tree-shaped wells (Liu et al., 2019), U-tube downhole (Lyu et 37al., 2018), and so on (Yan et al. 2019).

Although the previous simulation studies on heat extraction performance of different well 39layout are extensive, there is lack of a thorough and comprehensive comparison on heat extraction 40of application of oilfield injection scheme in HDR well layout. In this paper, the heat extraction 41performance of different well layout was investigated on the basis of the recovery and utilization 42of abandoned oil and water wells. Based on the injection scheme in oilfield, six ideal models for 43the HDR heat extraction are proposed. A thermal-hydraulic model is established to investigate the 44heat extraction performance of different well layout. Based on the model, the temperature 1 distribution, pressure distribution, average production temperature, life span, average rock 2 temperature and heat extraction ratio are proposed to evaluate the heat extraction performance of 3 different well layout, the heat extraction performance of different well layout are compared, the 4 effects of injection mass flow rate and injection temperature on the heat extraction performance 5 are studied. This study provides good guidance for the selection and optimization of different EGS 6 well layout.

7

8Methodology

9Model assumptions

10In this work, we focus on the heat extraction performance of EGS under different combination of 11fracture and well array. The computational model includes the following assumptions:

12 (1) The HDR reservoir rock is homogenous and isotropic. The density, porosity, permeability, 13heat conductivity and heat capacity at constant pressure of HDR reservoir rock consider to be 14constant under the heat extraction condition. The HDR reservoir is saturated with water before the 15heat extraction operation.

16 (2) The water keeps in liquid state under the heat extraction condition, because the pressure 17 and temperature meet the conditions of to keep it in liquid state (the specification of water phase 18 diagram see **Figure 1.**). The density, dynamic viscosity, heat conductivity and heat capacity at 19 constant pressure of water changes with temperature (see **Figure 2. – Figure 5.**).

20 (3) The permeability of the rock matrix is relatively lower, almost impermeable. Assuming 21there is a fracture between each injection well and production well as the key heat extraction 22channel. The fracture penetrates through the computational reservoir along corresponding the 23injection well and production well. The maximum distance among the injection well keeps 24consistent under different well layout. The reservoir descriptions of computational model are 25shown in **Table 2**.

26Mathematical equations

1

27The flow of water is laminar flow and subject to Darcy's law. Firstly, according to the mass 28conservation equation and Darcy law, the water flow in the porous media and the Darcy seepage 29velocity u can be described as (Liang et al., 2016)

$$\frac{\partial(\rho_{\rm w}\varepsilon_{\rm p})}{\partial t} + \nabla \cdot (\rho_{\rm w}u) = -Q_{\rm m} \tag{1}$$

31
$$u = -\frac{k}{\mu_w} (\nabla p + \rho_w g \nabla z)$$
(2)

32 where $\rho_{\rm w}$ denotes water density, $\mathcal{E}_{\rm p}$ denotes the rock matrix porosity, t denotes the time, ∇

33 denotes the Hamiltonian operator, u denotes the Darcy seepage velocity, Q_m denotes the source 34 term, which is the mass transfer between the rock matrix and fractures, k denotes the rock matrix 35 permeability, μ_w denotes water viscosity, P denotes the pressure and $\rho_w g \nabla z$ denotes the 36 gravity term.

The rock matrix is regarded as elastic porous storage and the effect of pressure on porosity is 38considered

$$\frac{\partial(\rho_{w}\varepsilon_{p})}{\partial t} = \varepsilon_{p}\frac{\partial\rho_{w}}{\partial t} + \rho_{w}\frac{\partial\rho_{w}}{\partial p}\frac{\partial p}{\partial t}$$
(3)

1 According to the state equation of the rock matrix, the rock compressibility can be described 2as

3
$$C_{\rm m} = \frac{1}{\varepsilon_{\rm p}} \frac{\partial \varepsilon_{\rm p}}{\partial p}$$
(4)

4 Define *S* as the storage coefficient of rock matrix and it can be described as

$$5 S = \varepsilon_p C_m (5)$$

6 Substituting Equation (2)-(5) into (1), the seepage field equation of water in the porous media 7 is obtained

8
$$\varepsilon_{p} \frac{\partial \rho_{w}}{\partial t} - \nabla \cdot \rho_{w} \left[\frac{k}{\mu} (\nabla p + \rho_{w} g \nabla z) \right] = -\rho_{w} S \frac{\partial p}{\partial t} - Q_{m}$$
(6)

9 Similarly, the seepage field equation of water in the fracture can be expressed as

10
$$d_{f}\varepsilon_{f}\frac{\partial\rho_{w}}{\partial t} - \nabla_{T} \cdot d_{f}\rho_{w}\left[\frac{k_{f}}{\mu}(\nabla_{T}p + \rho_{w}g\nabla_{T}z)\right] = -d_{f}\rho_{w}S_{f}\frac{\partial p}{\partial t} + d_{f}Q_{m}$$
(7)

11 where $d_{\rm f}$ denotes the fracture aperture, $\varepsilon_{\rm f}$ denotes the fracture porosity, $\nabla_{\rm T}$ denotes the 12gradient operator on the fracture's tangential plane, $k_{\rm f}$ denotes the fracture permeability and $S_{\rm f}$ 13denotes the storage coefficient of fracture.

From previous studies (Cao et al., 2016; Jiang et al., 2014), the local thermal equilibrium is 15applicable under the condition of the heat transfer coefficient and area is relatively large, the 16fracture aperture is relatively small. Therefore, in this work the local thermal equilibrium theory is 17adopted to investigate the temperature field.

According to the energy conservation equation, the heat transfer process in the porous media 19can be described as (Xu et al., 2015; Saeid et al., 2013)

20
$$(\rho C_{\rm p})_{\rm eff} \frac{\partial T}{\partial t} + \rho_{\rm w} C_{\rm p,w} u \cdot \nabla T - \nabla \cdot (\lambda_{\rm eff} \nabla T) = -Q_{\rm m,E}$$
(8)

21 where T denotes the temperature of porous media, $C_{p,w}$ denotes the water specific heat,

 $22 Q_{m,E}$ denotes the heat transfer between the porous media and fractures, $(\rho C_p)_{eff}$ denotes the 23 effective volumetric capacity, λ_{eff} denotes the effective thermal conductivity. According to the 24 volume average model, $(\rho C_p)_{eff}$ and λ_{eff} can be described as

25
$$(\rho C_{\rm p})_{\rm eff} = (1 - \varepsilon_{\rm p})\rho_{\rm s}C_{\rm p,s} + \varepsilon_{\rm p}\rho_{\rm w}C_{\rm p,w}$$
(9)

26
$$\lambda_{\rm eff} = (1 - \varepsilon_{\rm p})\lambda_{\rm s} + \varepsilon_{\rm p}\lambda_{\rm w}$$
(10)

27 where ρ_s denotes density of the rock matrix, $C_{p,s}$ and $C_{p,w}$ denote the specific heat of the 28rock matrix and water, λ_s and λ_w denote the thermal conductivity of the rock matrix and water, 29respectively.

30 Similarly, the heat transfer process in the fracture can be described as

1
$$d_{\rm f}(\rho C_{\rm p})_{\rm eff} \frac{\partial T}{\partial t} + d_{\rm f} \rho_{\rm w} C_{\rm p,w} u \cdot \nabla_{\rm T} T - \nabla_{\rm T} \cdot (d_{\rm f} \lambda_{\rm eff} \nabla T) = d_{\rm f} Q_{\rm m,E}$$
(11)

2Model and parameters under different well layout

3In this work, six ideal models are established for the HDR heat extraction according to the oil field 4 well layout. The case 1 is row opposite well layout, two production wells in the middle of 5 reservoir and four injection wells are located on opposite sides to the production well. The case 2 bis row cross well layout, two production wells in the middle of reservoir and six injection wells 7 cross with the production wells on both sides. The case3 is four-spot well layout, three injection 8 wells are located at the apex of an equilateral triangle with a side length of 400m and the 9production well is located at the center of the triangle. The case 4 is five-spot well layout, four 10injection wells are located at the apex of a square with a side length of 400m and the production 11 well is located at the center of the square. The case 5 is seven-spot well layout, six injection wells 12are located at the apex of the hexagon with a side length of 200m and the production well is 13located at the center of the hexagon. The case 6 is nine-spot well layout, eight injection wells are 14located at the apex and midpoint of the square with a side length of 400m and the production well 15 located at the center of the square. The six models differ greatly in well layout, but there are 16common points among different models. First, for each model, there is a fracture between each 17 injection well and production well as the key heat extraction channel, and the fracture penetrates 18through the reservoir along corresponding the injection well and production well. Second, the 19maximum distance among the injection well keeps consistent under different well layout and the 20maximum distance is set as 400m in this work.

The schematic of different well array and the computational model are shown in **Figure 6**. 22and **Figure 7**. respectively. The specific spatial descriptions of computational model are shown in 23**Table 2**.

The computational model mentioned above is adopted to simulate the heat extraction process 25of different well layout. The specific initial and boundary conditions are shown as below:

26 (1) The HDR reservoir rock initial temperature at the top is 473.15 K. The temperature 27 increases linearly with the depth and the geothermal gradient is 0.03 K/m. The initial temperature 28 of other outer boundaries can be calculated by the initial temperature at the top and the geothermal 29 gradient. The outer boundaries are set as thermal insulation.

30 (2) The HDR reservoir rock initial pressure at the top is 40 MPa. The pressure increases 31linearly with the depth and the pressure gradient is 0.005 MPa/m. The initial pressure of other 32outer boundaries can be calculated by the initial pressure at the top and the pressure gradient. Set 33production pressure to 30 MPa.

34 (3) The injection wells are set as inlet boundaries. The injection temperature is set as 293.15K 35and the injection mass flow rate is set as 120 kg/s. The production wells are set as outlet 36boundaries. The production pressure is set as 30 MPa.

37 The specific descriptions mentioned above can be seen in **Table 3**.

In order to guarantee the same simulation condition, adopting the same principle to mesh 39computational model under different well layout. All the domains adopt the free tetrahedral mesh. 40For the injection and production wells adopt the extra fine mesh and the maximum element size is 414m. The other domain adopts the fine mesh. The specific mesh descriptions of different well 42layout can be seen in **Table 4**. The mesh diagram of different well layout can be seen in **Figure 8**. 1 the legend represents the element size.

2Results and Discussion

3Temperature and pressure distribution

4In this section, the heat extraction performance of different well layout is compared under the total 5injection rate is 120 kg/s. **Figure 9.** and **Figure 10.** illustrate the temperature and pressure 6distribution of different well layout at 30th year. It can be observed that the heat extraction ratio 7and thermal residual position is different from case 1 to case 6. The production pressure keeps at 830 MPa and the injection pressure is much higher than production well to guarantee the fluid flow.

9 Since the total injection mass flow rate is the same, it can be speculated that the difference in 10temperature and pressure distribution is mainly caused by the combination of different well layout 11 and fractures.

The Darcy velocity field and pore pressure field on x-y plane of case 1 is shown in **Figure 11**. 13From **Figure 11**., it is found that the streamline and pressure contour near injection and production 14well is much denser than the rest of region. It indicates that the vicinity of injection and production 15well have higher velocity gradient and pressure gradient. Moreover, the pressure contours near the 16injection and production well are concentric circles, concluding that the wells are essentially 17boundaries of uniform pressure.

Driven by the pressure difference, working fluid flow from the injection well, through the 19rock matrix and fractures into the production well, thus the HDR heat extraction process can be 20realized. Compare the **Figure 11.** (a) and **Figure 11.** (b), it is found that where the pressure 21gradient small, the fluid flow velocity is small, it indicates that the fluid flow velocity mainly 22depends on the pressure gradient. Compare the **Figure 11.** and **Figure 8.**, it is found that the 23thermal residual region of case 1 is where both the pressure gradient and the fluid flow velocity 24are small. The law is also applicable to case 2 - case 6 and the pressure contour and streamline of 25case 2 - case 6 is shown in **Figure 12.** – **Figure 16**. From above, it can be concluded that the 26injection well number and the location of injection wells have critical influence on the thermal 27extraction performance. It is necessary to choose proper well layout according to actual demand. 28

29Average production temperature and life span

30**Figure17.** demonstrates the average production temperature and life span of different well layout 31under the total injection mass flow rate is 120 kg/s. From **Figure 17.**, it is found that the average 32production temperature declines with the heat extraction time increases, and the decline trend is 33different under different well layout. In the first 17 years, the average production temperature of 34case 3 is higher than other well layout and after the 17th year, the average production temperature 35of case 1 is the highest. The average production temperature of case 6 is always the lowest.

For case 2 and case 3, the injection-production wells ratio is the same (both are three), the 37 fracture area of case 2 is larger than that of case 3. In the first 19 years, the average temperature of 38 case 3 is higher than that of case 2 and after the 20th year, the result is contrary. It can be 39 speculated that the production temperature is related to the fracture area when the HDR energy is 40 enough, the smaller the fracture area, the higher the average production temperature.

For case 3 and case 5, the production well number and fracture area are same, the injection 42well number is three and six, respectively. In the first 21 years, the average temperature of case 3 43 is higher than that of case 5 and after the 22th year, the average temperature is almost the same. It

1 can be speculated that the production temperature is related to the injection well number when the 2HDR energy is enough, the fewer the injection well number, the higher the average production 3 temperature.

4 In the first few years, the HDR energy is enough, it is found that the average production 5 temperature is case 3, case 1, case 4, case 5, case 2 and case 6 from high to low, respectively. The 6 injection well number is 3, 4, 4, 6, 6 and 8, respectively. The fracture area is 8.3×10^5 , 5.0×10^5 , 77.1×10^5 , 8.3×10^5 , 11.2×10^5 and 12.1×10^5 m², respectively. From the data above, it can be 8 concluded that the injection well number is the key factor on the average production temperature. 9 When the injection well number is the same, the fracture area plays an important role on the 10 average production temperature. Both the injection well number and fracture area have a negative 11 effect on the average production temperature.

12 The average production temperature determines the life span of the enhanced geothermal 13system (EGS). The production temperature should be greater than 378.51 and 323.15 K to meet 14the electricity generation and heating demand, respectively. For electricity generation, the life span 15is 20.2, 19.2, 19.0, 19.2, 18.2 and 13.9 years from case 1 to case 6, respectively. For heating 16demand, the life span is 30.0, 30.0, 29.9, 30.0, 29.8, and 27.7 years case 1 to case 6, respectively. 17Since the maximum calculation time is 30 years, there may be errors in the life span statics for 18heating demand.

19Average rock temperature and heat extraction ratio

20The production mass flow rate is often used as an evaluation criterion in previous studies and it 21can be calculated by the velocity integral of specific two-dimension region in 3D model. The 22calculation result is different with the different integral region. For a certain well layout, we can 23choose a specific integral region (always the partial fracture region) to calculate the production 24mass flow rate and use it as an evaluation criterion for sensitivity analysis. However, in this work, 25the heat extraction of different well layout is mainly compared, there is no identical integral region 26to choose, and the calculation results of the production mass flow rate with different integral 27region cannot be put in the same standard for comparison.

Therefore, other characteristic parameters should be found to evaluate the heat extraction 29 process. The average rock temperature is a reliable characteristic parameter. The simulation model 30 is an ideal model and ignore the energy consumption. The lower the average rock temperature is, 31 the better the heat extraction effect is and the heat extraction ratio calculated by the average rock 32 temperature is more accurate. The definition of the heat extraction ratio η is given by

33
$$\eta = \frac{\iiint_{V} \rho_{s} C_{p,s} (T_{r0} - T_{r}(t)) dv}{\iiint_{V} \rho_{s} C_{p,s} (T_{r0} - T_{in}) dv}$$
(12)

34 where T_{r0} denotes the initial temperature of the porous matrix, $T_r(t)$ denotes the temperature

35 at time instant, T_{in} denotes the injection temperature.

Figure 18. demonstrates the average rock temperature and heat extraction ratio during 30 37 years of different well layout under the total injection mass flow rate is 120 kg/s. From **Figure 18.**, 38 it is found that the heat extraction ratio is case 3, case 1, case 4, case 5, case2 and case 6 from high 39 to low in the first 25 years, respectively. The results of heat extraction ratio are consistent with the

laverage production temperature.

In the last 5 years, the heat extraction ratio is case 1, case 3, case 4, case 5, case2 and case 6 3from high to low, respectively. The fracture area is 5.0×10^5 , 8.3×10^5 , 7.1×10^5 , 8.3×10^5 , 11.2×10^5 4and 12.1×10^5 m², respectively. If the simulation time is prolonged to 40 years, the heat extraction 5ratio of case 4 may surpass that of case 3. Therefore, it can be concluded that the injection well 6number is the key factor and the fracture area is the secondary factor on heat extraction when the 7HDR energy is enough, the influence of the injection well number is weakened and the fracture 8area is the key factor when the HDR energy is not enough.

9 Figure 19. demonstrates the heat extraction ratio for (a) Electricity generation and (b) 10Heating demand of different well layout under the total injection mass flow rate is 120 kg/s. Under 11the simulation condition, for electricity generation, the heat extraction ratio is 65.83, 57.35, 65.96, 1262.79, 59.30 and 43.09 % from case 1 to case 6, respectively. For heating demand, the heat 13extraction ratio is 78.91, 69.63, 77.02, 75.92, 72.27 and 58.94 %, respectively. Since the maximum 14calculation time is 30 years, there may be errors in the heat extraction statics for heating demand. 15Under the simulation condition, Case 1, Case 3 and Case 4 is the good choice both for electricity 16generation and heating demand.

17Effect of injection mass flow rate

18The simulation results above is calculated under the total injection mass flow rate is 120 kg/s, in 19this section, the injection mass flow rate of single well is set as 40 kg/s to compare the heat 20extraction process of different well layout.

Figure 20. demonstrates the average production temperature and heat extraction ratio of 22different well layout under the single well injection mass flow rate is 40 kg/s. From the **Figure 2320.**, we can see that average production temperature is case 3, case 1, case 4, case 5, case 2 and 24case 6 from high to low, respectively. The total injection mass flow rate is 120, 160, 160, 180, 180, 25320 kg/s, respectively. Under the same single well injection mass flow rate, the total injection 26mass flow rate depends on the injection well number, the more the injection wells, the lower the 27average production temperature and the shorter the time to reach a stable temperature. When the 28injection well number is the same, the fracture area plays an important role on the average 29production temperature. The larger the fracture area, the lower the average production 30temperature. The injection well number determines the average production temperature in the 31whole process.

Figure 21. demonstrates the heat extraction ratio for (a) Electricity generation and (b) 33Heating demand of different well layout under the single well injection mass flow rate is 40 kg/s. 34Under the simulation condition, for electricity generation, the life span and heat extraction ratio 35are 14.8, 8.2, 19.0, 14.1, 8.5, 4.6 years and 65.20, 53.40, 65.96, 62.31, 57.64, 40.50 % from case 1 36to case 6, respectively. For heating demand, the life span and heat extraction ratio are 20.2, 19.2, 3719.0, 19.2, 18.2, 13.9 years and 81.90, 69.13, 77.02, 77.28, 72.18 and 58.21 %, respectively. Since 38the maximum calculation time is 30 years, there may be errors in the heat extraction statics for 39heating demand.

40 From the static results above, it is found that the total injection mass flow rate has negative 41 effect on the life span and heat extraction ratio for the same well layout. Under the simulation 42 condition, Case 1, Case 3 and Case 4 is the good choice both for electricity generation and heating 43 demand.

1Effect of injection temperature

2Figure 22. compares the average production temperature and heat extraction ratio under the 3injection temperature is 293.15 and 303.15 K. For case 1, when the injection temperature increases 4from 293.15 to 303.15 K, the life span for electricity generation is extended from 20.2 to 20.9 5years and the heat extraction ratio decreased from 65.82 to 62.79. The same law can be found in 6case 2 to case 6, too. The higher the injection temperature, the lower the average production 7temperature and the heat extraction ratio. The low injection temperature is beneficial to the heat 8extraction for all the cases. The heat extraction ratio of Case1, Case 3 and Case 4 is greatly 9affected by the injection temperature.

10Conclusions

11In this paper, six EGS well layout schemes are proposed based on the utilization of abandoned oil-12water wells and common oilfield well pattern. Six common injection-production well pattern in 13oilfield are combined to HDR production and the heat extraction performance is simulated. A 14thermal-hydraulic model is established to investigate the heat extraction performance of different 15well layout. Based on the model, the temperature distribution, pressure distribution, average 16production temperature, life span, average rock temperature and heat extraction ratio are proposed 17to evaluate the heat extraction performance of different well layout, the heat extraction 18performance of different well layout are compared, the effects of injection mass flow rate and 19injection temperature on the heat extraction performance are studied. In summary, the key points 20this work includes:

21 (1) Six ideal models for the HDR heat extraction are proposed based on the recovery and 22utilization of abandoned oil and water wells. The models are row opposite, row cross, four-spot, 23five-spot, seven-spot and nice-spot well layout from case 1 to case 6, respectively.

24 (2) The vicinity of injection and production well have higher velocity gradient and pressure 25gradient. The fluid flow velocity mainly depends on the pressure gradient and the thermal residual 26region is where both the pressure gradient and the fluid flow velocity are small. The injection well 27number and the location of injection wells have critical influence on the heat extraction 28performance. It is necessary to choose proper well layout according to actual demand.

(3) Under the same total injection mass flow rate, the injection well number is the key factor 30and the fracture area is the secondary factor on heat extraction when the HDR energy is enough, 31the influence of the injection well number is weakened and the fracture area is the key factor when 32the HDR energy is not enough. Both the injection well number and fracture area have a negative 33effect on the average production temperature. Under the same total injection mass flow rate, Case 341, Case 3 and Case 4 is the good choice both for electricity generation and heating demand. For 35electricity generation, the life span is 20.2, 19.2, 19.0, 19.2, 18.2 and 13.9 years, the heat 36extraction ratio is 65.83, 57.35, 65.96, 62.79, 59.30 and 43.09 % from case 1 to case 6, 37respectively. For heating demand, the life span is 30.0, 30.0, 29.9, 30.0, 29.8, and 27.7 years, the 38heat extraction ratio is 78.91, 69.63, 77.02, 75.92, 72.27 and 58.94 % from case 1 to case 6, 39respectively.

40 (4) Under the same single injection mass flow rate, the total injection mass flow rate depends 41on the injection well number, the more the injection wells, the lower the average production 42temperature and the shorter the time to reach a stable temperature. Under the same single well 43injection mass flow rate, Case 1, Case 3 and Case 4 is the good choice both for electricity 1 generation and heating demand. Under the same total injection mass flow rate, the higher the 2 injection temperature, the lower the average production temperature and the heat extraction ratio. 3 The heat extraction ratio of Case1, Case 3 and Case 4 is greatly affected by the injection 4 temperature.

5 However, the hydraulic-mechanical couple is not taken into consideration in this paper, the 6heat extraction performance of six EGS well layout need further study in the future.

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9Declaration of conflicting interests

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13 14 15

16**ORCID iD**

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18 Appendix

Case 1	Row opposite well layout
Case 2	Row cross well layout
Case 3	Four-spot well layout
Case 4	Five-spot well layout
Case 5	Seven-spot well layout
Case 6	Nine-spot well layout
C_{m}	Rock compressibility, Pa ⁻¹
$C_{\mathrm{p,w}}$	Water specific heat, $J/(kg \cdot K)$
$C_{\mathrm{p,s}}$	Rock matrix specific heat, $J/(kg \cdot K)$
$d_{ m f}$	Fracture aperture, m
EGS	Enhanced Geothermal System

HDR	Hot Dry Rock
k	Rock matrix permeability, m ²
$k_{ m f}$	Fracture permeability, m ²
р	Pressure, Pa
$Q_{ m m}$	the mass transfer between the rock matrix and fractures
$Q_{\mathrm{m,E}}$	the heat transfer between the porous media and fractures
S	Storage coefficient of rock matrix, Pa ⁻¹
$S_{ m f}$	Storage coefficient of fracture, Pa ⁻¹
t	Time, s
Т	Temperature of porous media, K
T _{in}	Injection temperature, K
T _p	Average production temperature, K
Tr	Average rock temperature, K
T _{ro}	Initial temperature of the porous matrix, K
и	Darcy seepage velocity, m/s
$ ho_{ m s}$	Rock matrix density, kg/m ³
$ ho_{ m w}$	Water density, kg/m ³
$(ho C_{ m p})_{ m eff}$	Effective volumetric capacity,
$\mu_{ m w}$	Water viscosity, Pa·s
\mathcal{E}_{f}	Fracture porosity, %
\mathcal{E}_{p}	Rock matrix porosity, %
∇	Hamiltonian operator
∇_{T}	gradient operator on the fracture's tangential plane
λ_{eff}	Effective thermal conductivity, $W/(m \cdot K)$
$\lambda_{\rm s}$	Thermal conductivity of rock matrix, $W/(m \cdot K)$
$\lambda_{ m w}$	Thermal conductivity of water, $W/(m \cdot K)$
η	Heat extraction ratio, %

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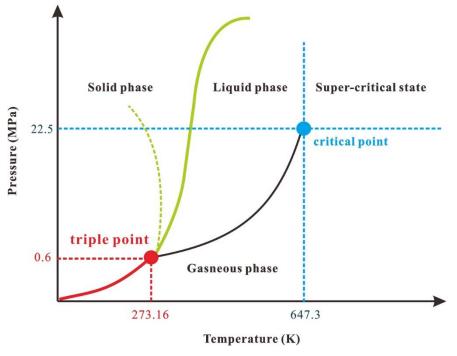
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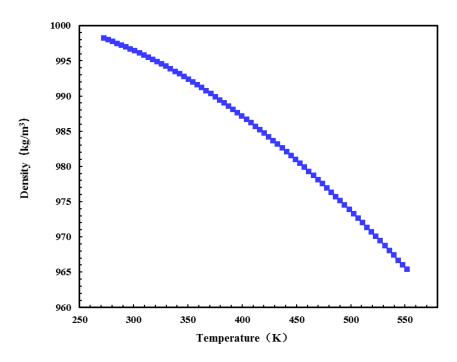
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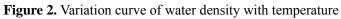
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23Figure captions







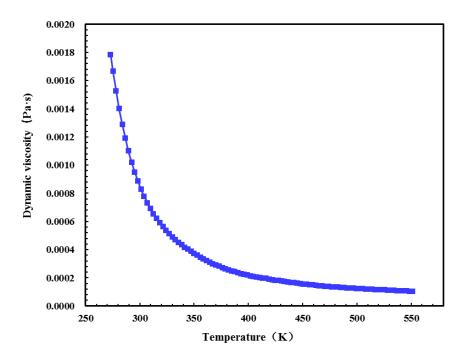


Figure 3. Variation curve of water dynamic viscosity with temperature

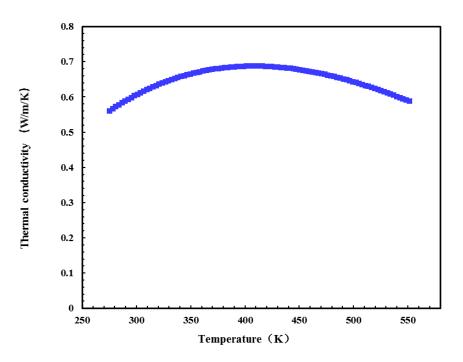


Figure 4. Variation curve of water thermal conductivity with temperature

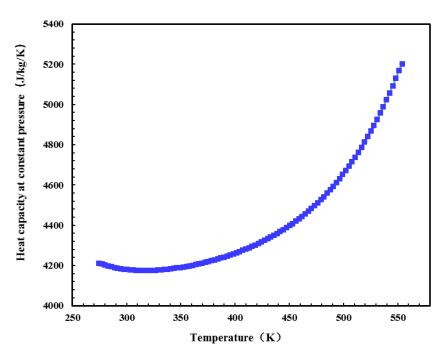




Figure 5. Variation curve of water heat capacity at constant pressure with temperature

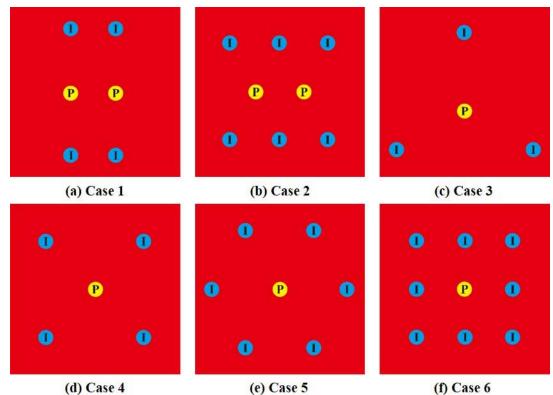
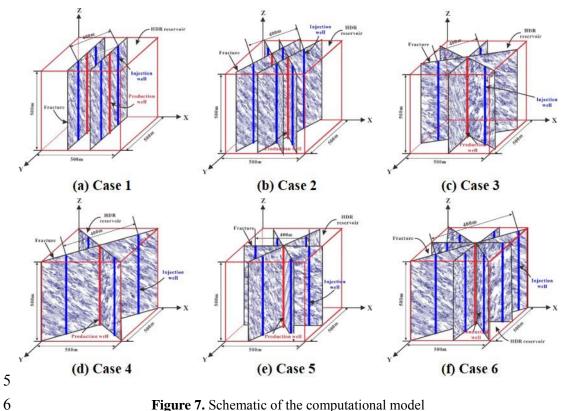
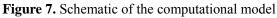


Figure 6. Schematic of different well array

Note: in the Figure 6, the red area represents HDR reservoir, the blue circles represent 4injection wells and the yellow circle represent production wells.





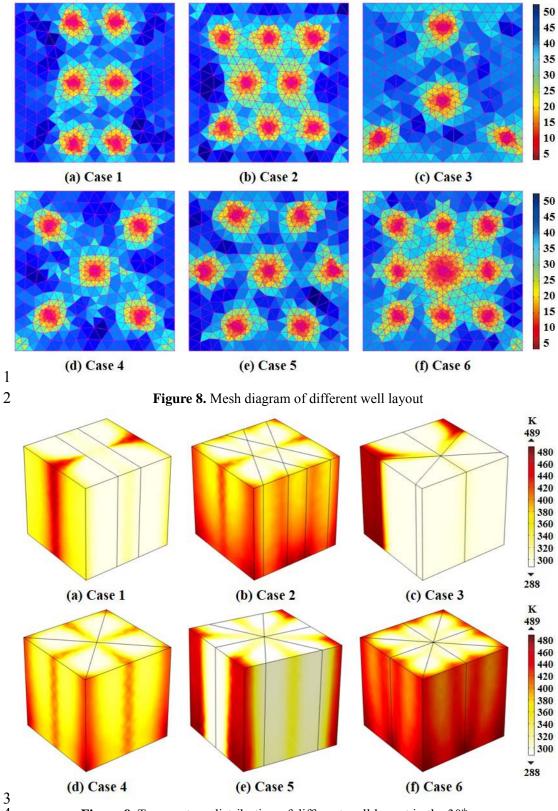
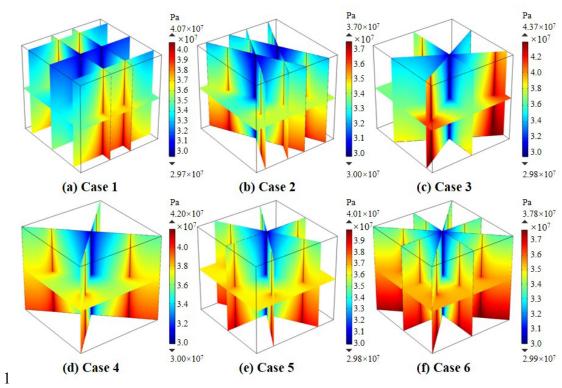




Figure 9. Temperature distribution of different well layout in the 30^{th} year



2

Figure 10. Pressure distribution of different well layout in the 30th year

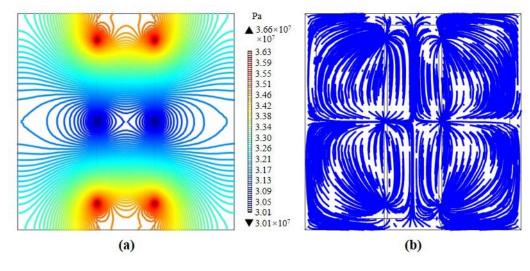




Figure 11. (a) Pressure contour; (b) Streamline of Case 1 in the 30th year

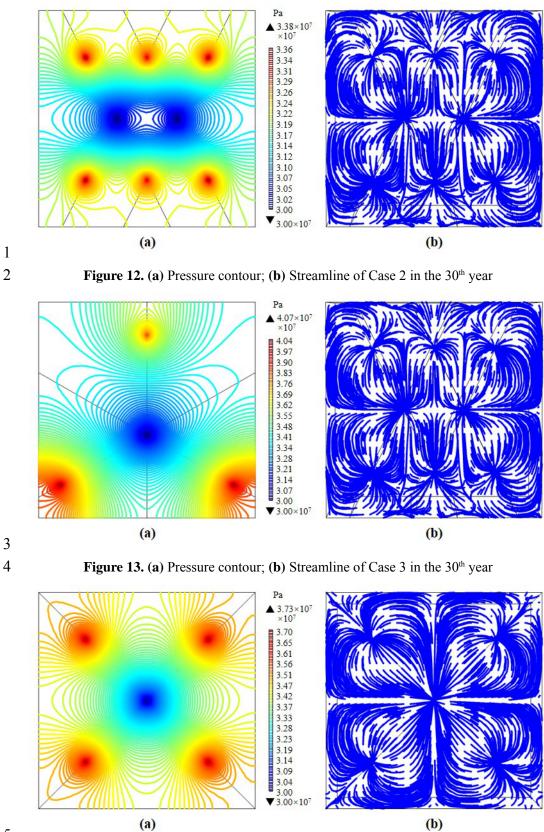




Figure 14. (a) Pressure contour; (b) Streamline of Case 4 in the 30th year

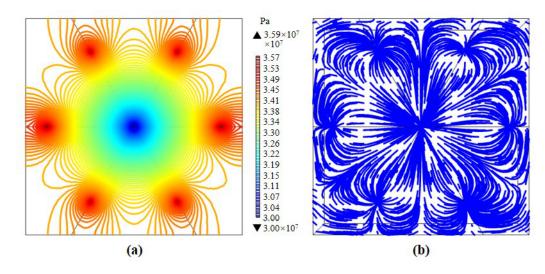




Figure 15. (a) Pressure contour; (b) Streamline of Case 5 in the 30th year

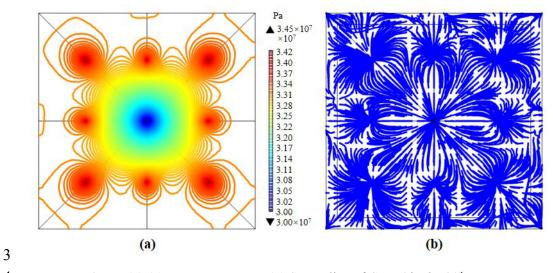
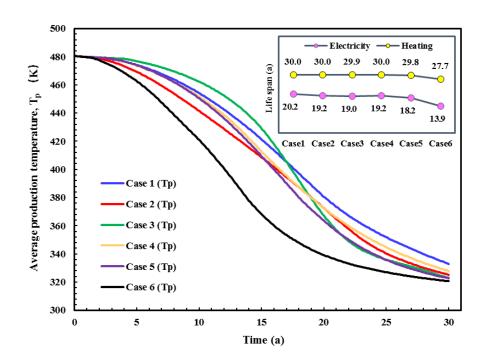
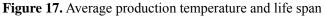


Figure 16. (a) Pressure contour; (b) Streamline of Case 6 in the 30th year





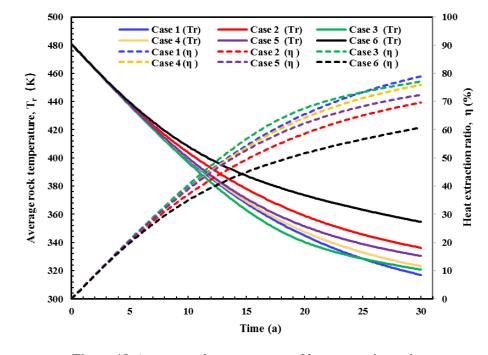




Figure 18. Average rock temperature and heat extraction ratio

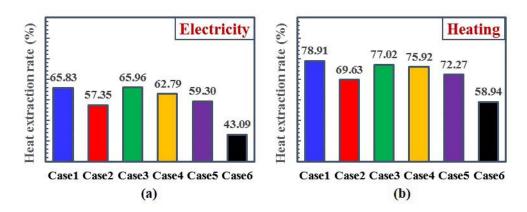


Figure 19. Heat extraction ratio for (a) Electricity generation and (b) Heating demand

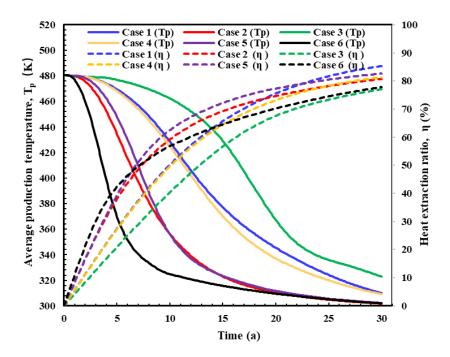
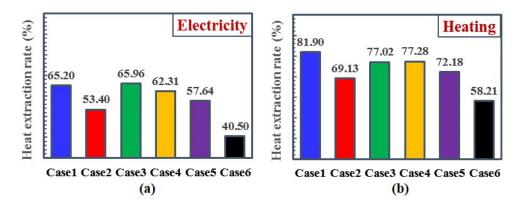
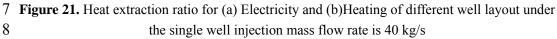


Figure 20. Average production temperature and heat extraction ratio under the single well injection mass flow rate is 40 kg/s





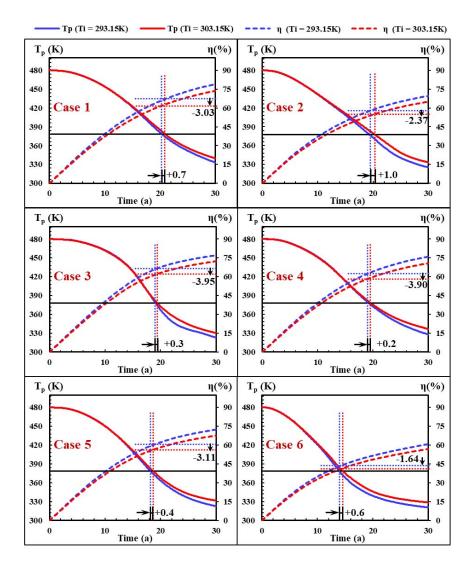




Figure 22. Comparison of average production temperature and heat extraction ratio under the
 injection temperature is 293.15 K and 303.15 K

4Tables

Description	HDR	Fracture	Unit	
Density	2700	2000	kg/m ³	
Porosity	0.08	1	%	
Permeability	10e-15	10e-11	m^2	
Heat conductivity	2.8	2.8	W/(m·K)	
Heat capacity at constant pressure	1000 850		$J/(kg \cdot K)$	
5 7 Table 2. The sp	atial description	ons of computational n	nodel	
Description Case 1	Case 2	Case 3 Case 4	Case 5 Case 6	

HDR dimensions			500m×50	00m×500m		
Injection well number	4	6	3	4	6	8
Production well number	2	2	1	1	1	1
Well diameter	1m	1m	1m	1m	1m	1m
Well length	500m	500m	500m	500m	500m	500m
Maximum well spacing	400m	400m	400m	400m	400m	400m
Fracture number	2	4	3	2	3	4
Fracture aperture	0.001m	0.001m	0.001m	0.001m	0.001m	0.001m
Fracture height	500m	500m	500m	500m	500m	500m
Table 3. The c	orrespondi	ing descript	ions of initia	l and bound	lary condition	ons
Description			Value		Unit	
Initial temperature at the te	op boundar	у	473.15		K	
Geothermal gradient			0.03		K/m	
Injection temperature Initial pressure at the top boundary			293.15 K 40 MPa			
Pressure gradient			0.005		MPa/m	
Production pressure			30		MPa	
Injection mass flow rate			120		kg/s	
	Table	4. Mesh of	different we	ll layout		
Description	Case 1	Case 2	Case 3	Case 4	Case 5	Case 6
Minimum element quality	0.2139	0.1901	0.1956	0.212	0.149	0.1835
Average element quality	0.6379	0.636	0.6406	0.6394	0.6344	0.6381
Tetrahedron	137218	184761	102601	123124	154738	220493
Triangle	14072	24628	14254	15034	19514	29664
Edge element	1102	1540	912	972	1341	1685