

Fig.S1 The TG and DTG curves of typical medical waste pyrolysis

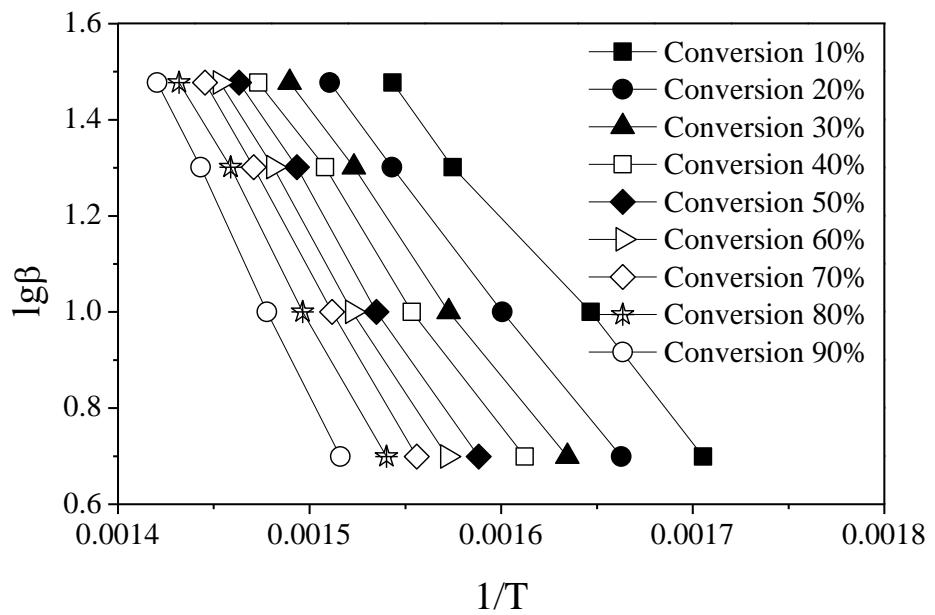


Fig. S2 The correlation of  $\lg\beta$  versus  $1/T$  at different conversion

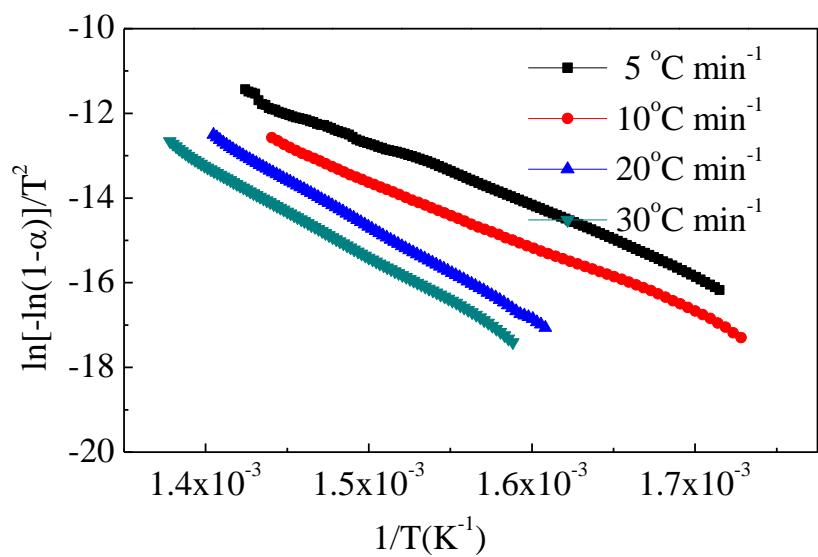


Fig. S3 The correlation of  $\ln[-\ln(1-\alpha)]/T^2$  versus  $1/T$  at different heating rate

**Table S1** Most common reaction models for heterogeneous reaction.

Symbol	Reaction mechanism	f(x)	G(x)
G1	One-dimensional diffusion	$1/2x$	$x^2$
G2	Two-dimensional diffusion (Valensi)	$[-\ln(1-x)]^{-1}$	$x + (1-x)\ln(1-x)$
G3	Three-dimensional diffusion (Jander)	$1.5(1-x)2/3[1-(1-x)1/3]^{-1}$	$[1-(1-x)1/3]^2$
G4	Three-dimensional diffusion (G-B)	$1.5[1-(1-x)1/3]^{-1}$	$1-2x/3-(1-x)^{2/3}$
G5	Three-dimensional diffusion (A-J)	$1.5(1+x)2/3[(1+x)1/3-1]^{-1}$	$[(1+x)1/3-1]^2$
G6	Nucleation and growth ( $n=2/3$ )	$1.5(1-x) [-\ln(1-x)]^{1/3}$	$[-\ln(1-x)]^{2/3}$
G7	Nucleation and growth ( $n=1/2$ )	$2(1-x) [-\ln(1-x)]^{1/2}$	$[-\ln(1-x)]^{1/2}$
G8	Nucleation and growth ( $n=1/3$ )	$3(1-x) [-\ln(1-x)]^{2/3}$	$[-\ln(1-x)]^{1/3}$
G9	Nucleation and growth ( $n=1/4$ )	$4(1-x) [-\ln(1-x)]^{1/4}$	$[-\ln(1-x)]^{1/4}$
G10	Autocatalytic reaction	$x (1-x)$	$\ln[x/(1-x)]$
G11	Mampel power law ( $n=1/2$ )	$2x^{1/2}$	$x^{1/2}$
G12	Mampel power law ( $n=1/3$ )	$3x^{2/3}$	$x^{1/3}$
G13	Mampel power law ( $n=1/4$ )	$4x^{3/4}$	$x^{1/4}$
G14	Chemical reaction ( $n=3$ )	$(1-x)^3$	$[(1-x)^{-2}-1]/2$
G15	Chemical reaction ( $n=2$ )	$(1-x)^2$	$(1-x)^{-1}-1$
G16	Chemical reaction ( $n=1$ )	$1-x$	$-\ln(1-x)$
G17	Chemical reaction ( $n=0$ )	$1$	$x$
G18	Contraction sphere	$3(1-x)^{2/3}$	$1-(1-x)^{1/3}$
G19	Contraction cylinder	$2(1-x)^{1/2}$	$1-(1-x)^{1/2}$

**Note:** A-J: Anti-Jander; G-B: Ginstling-Brounshtein.

**Table S2** Probable reaction models and kinetics parameters for H<sub>2</sub> during medical waste pyrolysis in MFBR

Temperature	G(X)	G3	G7	G8	G16
700 °C	lnK(T)	-4.2131	-2.9917	-3.3326	-2.2624
	R <sup>2</sup>	0.9178	0.7422	0.6755	0.9784
750 °C	lnK(T)	-4.0008	-2.7395	-3.0791	-2.0371
	R <sup>2</sup>	0.9299	0.7797	0.7229	0.9348
800 °C	lnK(T)	-3.7593	-2.5059	-2.8525	-1.7934
	R <sup>2</sup>	0.9053	0.7848	0.7378	0.9495
850 °C	lnK(T)	-2.9720	-1.7243	-2.1078	-0.9856
	R <sup>2</sup>	0.9429	0.9355	0.8927	0.9850
900 °C	lnK(T)	-2.9041	-1.6476	-1.9668	-0.9522
	R <sup>2</sup>	0.9823	0.9726	0.9293	0.9918
<b>E<sub>a</sub> (kJ·mol<sup>-1</sup>)</b>		<b>68.84</b>	<b>72.34</b>	<b>69.96</b>	<b>69.39</b>
<b>A (s<sup>-1</sup>)</b>		<b>65.42</b>	<b>342.13</b>	<b>182.78</b>	<b>495.12</b>

**Table S3** Probable reaction models and kinetics parameters for CH<sub>4</sub> during medical waste pyrolysis in MFBR.

Temperature	G(X)	G3	G7	G8	G16
700 °C	lnK(T)	-3.4082	-1.8637	-2.1345	-1.3471
	R <sup>2</sup>	0.9103	0.896	0.8772	0.9214
750 °C	lnK(T)	-3.2416	-1.6650	-1.9303	-1.1023
	R <sup>2</sup>	0.9144	0.9434	0.9346	0.9419
800 °C	lnK(T)	-2.8860	-1.4254	-1.6933	-0.8620
	R <sup>2</sup>	0.9422	0.9650	0.9138	0.9923
850 °C	lnK(T)	-2.6941	-1.2758	-1.5736	-0.7189
	R <sup>2</sup>	0.9527	0.8991	0.8466	0.9646
900 °C	lnK(T)	-2.5718	-1.1855	-1.6140	-0.4805
	R <sup>2</sup>	0.9809	0.9660	0.9312	0.9954
<b>E<sub>a</sub> (kJ·mol<sup>-1</sup>)</b>		<b>42.29</b>	<b>33.34</b>	<b>27.01</b>	<b>40.21</b>
<b>A (s<sup>-1</sup>)</b>		<b>6.05</b>	<b>9.68</b>	<b>3.50</b>	<b>37.50</b>

**Table S4** Probable reaction models and kinetics parameters for C<sub>2</sub>H<sub>2</sub> during medical waste pyrolysis in MFBR

Temperature	G(X)	G3	G7	G8	G16
700 °C	lnK(T)	-2.7333	-1.7649	-1.8669	-0.8151
	R <sup>2</sup>	0.9260	0.9596	0.9360	0.9595
750 °C	lnK(T)	-2.5145	-1.3224	-1.6414	-0.5490
	R <sup>2</sup>	0.9652	0.9684	0.9355	0.9991
800 °C	lnK(T)	-2.3666	-1.0255	-1.3637	-0.4917
	R <sup>2</sup>	0.9348	0.9634	0.9011	0.9651
850 °C	lnK(T)	-2.0746	-0.6962	-1.1351	-0.3274
	R <sup>2</sup>	0.9608	0.9240	0.8668	0.9805
900 °C	lnK(T)	-1.6863	0.5322	-0.9115	-0.0483
	R <sup>2</sup>	0.9260	1.0000	0.9833	0.9338
<b>E<sub>a</sub> (kJ·mol<sup>-1</sup>)</b>		<b>47.60</b>	<b>59.05</b>	<b>45.85</b>	<b>33.16</b>
<b>A (s<sup>-1</sup>)</b>		<b>21.83</b>	<b>264.83</b>	<b>43.70</b>	<b>26.75</b>

**Table S5** Probable reaction models and kinetics parameters for C<sub>2</sub>H<sub>4</sub> during medical waste pyrolysis in MFBR

Temperature	G(X)	G3	G7	G8	G16
700 °C	lnK(T)	-3.7722	-2.4476	-2.7457	-1.8547
	R <sup>2</sup>	0.9209	0.7937	0.7493	0.9347
750 °C	lnK(T)	-3.5032	-2.3046	-2.6145	-1.6836
	R <sup>2</sup>	0.9227	0.8312	0.7836	0.9050
800 °C	lnK(T)	-3.2289	-1.9414	-2.4805	-1.4192
	R <sup>2</sup>	0.9439	0.8617	0.7500	0.9103
850 °C	lnK(T)	-2.8932	-1.3591	-1.6363	-1.1725
	R <sup>2</sup>	0.9864	0.9231	0.8626	0.9995
900 °C	lnK(T)	-2.6607	-1.0876	-1.1815	-1.0350
	R <sup>2</sup>	0.9783	0.8977	0.8672	0.9707
<b>E<sub>a</sub> (kJ·mol<sup>-1</sup>)</b>		<b>53.69</b>	<b>69.01</b>	<b>76.60</b>	<b>40.82</b>
<b>A (s<sup>-1</sup>)</b>		<b>16.99</b>	<b>380.20</b>	<b>662.82</b>	<b>23.61</b>

**Table S6** Probable reaction models and kinetics parameters for C<sub>2</sub>H<sub>6</sub> during medical waste pyrolysis in MFBR

Temperature	G(X)	G3	G7	G8	G16
700 °C	lnK(T)	-3.4577	-2.6145	-2.9662	-1.7418
	R <sup>2</sup>	0.8921	0.7779	0.7263	0.8977
750 °C	lnK(T)	-3.2493	-2.2164	-2.5587	-1.4714
	R <sup>2</sup>	0.9221	0.8025	0.7437	0.9142
800 °C	lnK(T)	-2.9169	-1.6079	-2.1733	-1.1963
	R <sup>2</sup>	0.9558	0.9082	0.8508	0.9684
850 °C	lnK(T)	-2.7105	-1.4749	-1.8432	-0.9787
	R <sup>2</sup>	0.9523	0.8771	0.8419	0.9427
900 °C	lnK(T)	-2.6105	-1.1466	-1.7131	-0.8470
	R <sup>2</sup>	0.9997	0.9484	0.9041	1.000
<b>E<sub>a</sub> (kJ·mol<sup>-1</sup>)</b>		<b>42.61</b>	<b>70.23</b>	<b>61.58</b>	<b>43.54</b>
<b>A (s<sup>-1</sup>)</b>		<b>6.10</b>	<b>443.01</b>	<b>107.90</b>	<b>38.65</b>

**Table S7** Probable reaction models and kinetics parameters for C<sub>3</sub>H<sub>6</sub> during medical waste pyrolysis in MFBR

Temperature	G(X)	G3	G7	G8	G16
700 °C	lnK(T)	-3.4610	-2.3166	-2.6479	-1.4784
	R <sup>2</sup>	0.9414	0.8201	0.7528	0.9240
750 °C	lnK(T)	-3.2416	-1.9980	-2.2946	-1.2870
	R <sup>2</sup>	0.9571	0.8782	0.7978	0.9600
800 °C	lnK(T)	-2.9858	-1.4974	-1.7778	-1.0527
	R <sup>2</sup>	0.9458	0.9525	0.8958	0.9727
850 °C	lnK(T)	-2.7536	-1.3171	-1.7209	-0.8160
	R <sup>2</sup>	0.9340	0.9951	0.9757	0.9667
900 °C	lnK(T)	-2.5536	-1.0692	-1.3677	-0.5989
	R <sup>2</sup>	0.8737	0.9859	0.9905	0.9650
<b>E<sub>a</sub> (kJ·mol<sup>-1</sup>)</b>		<b>43.69</b>	<b>60.58</b>	<b>59.80</b>	<b>42.21</b>
<b>A (s<sup>-1</sup>)</b>		<b>6.81</b>	<b>177.81</b>	<b>117.9</b>	<b>40.64</b>

**Table S8** Probable reaction models and kinetics parameters for C<sub>3</sub>H<sub>8</sub> during medical waste pyrolysis in MFBR

Temperature	G(X)	G3	G7	G8	G16
700 °C	lnK(T)	-5.8781	-4.5952	-5.0056	-4.0063
	R <sup>2</sup>	0.9208	0.9870	0.9771	0.9634
750 °C	lnK(T)	-5.5468	-4.3351	-4.7330	-3.6969
	R <sup>2</sup>	0.9615	0.9588	0.9171	0.9883
800 °C	lnK(T)	-5.3602	-4.2687	-4.6777	-3.4389
	R <sup>2</sup>	0.9724	0.9478	0.9128	0.9818
850 °C	lnK(T)	-5.0207	-3.9954	-4.4228	-3.2289
	R <sup>2</sup>	0.9953	0.9183	0.8813	0.9747
900 °C	lnK(T)	-4.8159	-3.4142	-3.8444	-2.8896
	R <sup>2</sup>	0.9947	0.9104	0.8701	0.9815
<b>E<sub>a</sub> (kJ·mol<sup>-1</sup>)</b>		<b>50.32</b>	<b>50.47</b>	<b>49.20</b>	<b>51.19</b>
<b>A (s<sup>-1</sup>)</b>		<b>1.41</b>	<b>4.76</b>	<b>2.72</b>	<b>10.08</b>

**Table S9** Probable reaction models and kinetics parameters for C<sub>4</sub>H<sub>4</sub> during medical waste pyrolysis in MFBR

Temperature	G(X)	G3	G7	G8	G16
700 °C	lnK(T)	-4.7330	-3.8258	-2.0341	-0.7221
	R <sup>2</sup>	0.9043	0.7963	0.7241	0.9335
750 °C	lnK(T)	-4.5854	-3.4327	-1.5385	-0.5295
	R <sup>2</sup>	0.9402	0.8748	0.7940	0.9582
800 °C	lnK(T)	-4.4567	-3.2089	-1.0131	-0.03542
	R <sup>2</sup>	0.9826	0.9514	0.8944	0.9724
850 °C	lnK(T)	-3.8680	-2.9604	-0.9524	0.2937
	R <sup>2</sup>	0.9855	0.9951	0.9757	0.9667
900 °C	lnK(T)	-3.4673	-2.7303	-0.6079	0.4448
	R <sup>2</sup>	0.9755	0.9844	0.9905	0.9909
<b>E<sub>a</sub> (kJ·mol<sup>-1</sup>)</b>		<b>60.70</b>	<b>50.74</b>	<b>65.85</b>	<b>60.02</b>
<b>A (s<sup>-1</sup>)</b>		<b>13.61</b>	<b>11.95</b>	<b>484.73</b>	<b>770.93</b>

**Table S10** Probable reaction models and kinetics parameters for mixed gas during medical waste pyrolysis in MFBR

Temperature	G(X)	G3	G7	G8	G16
700 °C	lnK(T)	-4.8158	-2.9759	-3.4577	-2.6310
	R <sup>2</sup>	0.9395	0.9927	0.9687	0.9696
750 °C	lnK(T)	-4.5375	-2.6200	-3.3326	-2.3309
	R <sup>2</sup>	0.9748	0.9748	0.9231	0.9868
800 °C	lnK(T)	-4.2831	-2.6245	-3.1820	-2.1421
	R <sup>2</sup>	0.9679	0.9472	0.8964	0.9933
850 °C	lnK(T)	-4.0513	-2.0129	-2.9431	-1.7418
	R <sup>2</sup>	0.9778	0.9327	0.8738	0.9942
900 °C	lnK(T)	-3.7507	-1.7441	-2.8150	-1.5177
	R <sup>2</sup>	0.9768	0.9663	0.8123	0.9560
<b>E<sub>a</sub> (kJ·mol<sup>-1</sup>)</b>		<b>49.56</b>	<b>57.82</b>	<b>31.65</b>	<b>53.30</b>
<b>A (s<sup>-1</sup>)</b>		<b>3.64</b>	<b>61.27</b>	<b>1.52</b>	<b>50.79</b>